

Agenda



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Project Overview

8 June 2022





Project in Brief





In an Australian-first 43 kilometres of Parmelia Gas Pipeline (PGP) will be transformed to 100 percent hydrogen-ready transmission pipeline.



The project is supported by The Future Fuels Cooperative Research Centre, Wollongong University and GPA Engineering.



The project will provide information into the pipeline industry hydrogen body of knowledge – supporting the H2 Pipeline CoP

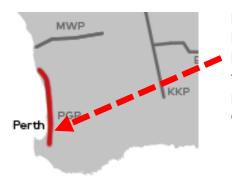


The project will be delivered in three phases – testing, transformation and commissioning

APA is committed to working with the regulator and State Government to demonstrate the safety case for hydrogen



Research team preparing pipe sections for testing



Kwinana is a key potential hydrogen production location, linked to a large industrial base, domestic network and transport hubs, with the potential to one day service export markets.





Project Need, Challenges & Approach



Phase 1: Investigate if the pipeline can transport hydrogen

- Complete gap analysis of current standards
- Prepare safety management approach
- Collate existing pipeline data incl. properties and current condition
- Conduct laboratory testing of pipe sections in air at atmospheric pressure

Phase 2: Confirm how to convert the pipeline to hydrogen-ready

- o Finalise safety management study
- Engage with technical regulator and WA State Government
- Complete supply and demand analysis and commence negotiations
- Conduct laboratory testing of pipe sections in a gaseous hydrogen environment

Phase 3: Prepare the pipeline for transformation

- Full-scale testing if required
- Assessment and conversion of above-ground and ancillary equipment changes required for hydrogen-ready
- Firm understanding of supply and offtake arrangements incl. points of connection





Laboratory Test Program



General information on the PGP Kwinana section				
Material specification	API 5L			
Grade	X52			
Diameter	355.6			
Wall thickness	5.56, 7.92 mm			
SMYS	360 MPa			
SMTS	460 MPa			
Allowances	0 mm			
Length	42.3 km			
Location classses (AS 2885.6)	T1, T2 and R2			
Design temperature range	-7 to 65 °C			
Year of construction	Circa 1970			
Original design code	ANSI B31.8 (probably 1968 Ed.)			













Overview





All test are conducted in *air* at ambient temperature

Vintage pipe so testing required to fill in gaps



- Chemical Composition (OES)
- Optical Macro- & Micrographs
- Seam & Girth Weld Hardness Maps

Strength

- Base Metal Circumferential & Longitudinal Tensile Tests
- Cross Seam & Girth Weld Tensile Tests













Fracture Toughness

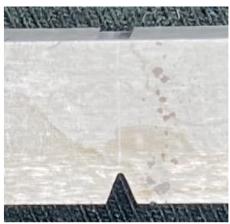
- Static Fracture
 - Base Metal Circumferential & Longitudinal C(T) Tests
 - Cross Girth Weld C(T) Tests in the HAZ & WCL
- Dynamic Fracture
 - Base Metal Circumferential Charpy V-notch Impact Tests
 - Seam Weld Charpy V-notch Impact Tests
 - Base Metal Circumferential DWTTs

Fatigue

- Base Metal Circumferential & Longitudinal C(T) Tests
- Cross Girth Weld C(T) Tests in the HAZ & WCL















Laboratory Testing



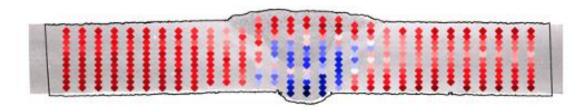


Chemical Composition

- Mostly fits modern specifications API 5L PSL2 X52N welded pipes
 - Section S8-E had %wt phosphorus and C_{eq} fell outside specifications
- ASME B31.12 option B requires phosphorous ≤0.015%wt
 - Some pipes above the limit

Material Hardness

- AS2885.2 Cl. 6.4.6
 - 350 HV in non-sour service
 - 250 HV in sour service
- ASME B31.12 Cl. GR-3.10
 - 235 HV, 1.5 mm below surface
- BM, HAZ and WM met requirements







Strength

- API 5L PSL2 (X52)
- AS/NZS 2885.2
 - TS of GW > SMTS of BM
- All specimens met requirements

Drop Weight Tear Test

- API 5L & ISO 3183 do not require DWTTs for < DN500
- AS 2885.1 requires FATT(85%) < TBFC (-10 °C)
- ASME B31.12 requires %SA > 40% at TBFC
- All specimens met requirements





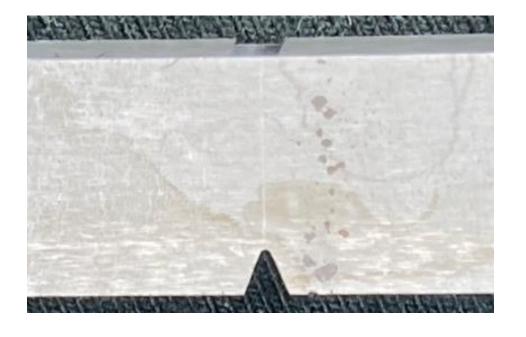






Charpy V-notch Impact Test

- AS 2885.1
 - Min 27 J for pipe metal
 - Higher as part of the FCP for initiation and propagation
 - HFW seam meet requirements for fracture initiation in HCA in WCL only
- ASME B31.12
 - Min 27 J for WM and HAZ
- BM & HAZ specimens met requirements
- SW centreline did not (vintage steel)

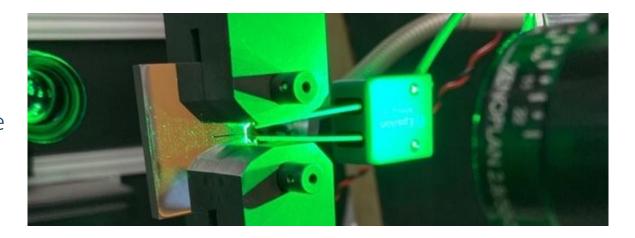


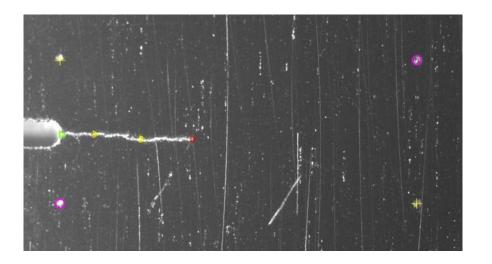




Fatigue Test (ASTM E647)

- Not typically seen as issue with NG pipeline
- Critical to have the FCGR in H₂ to assess remaining life based on operating scenarios
- Results consistent with literature
- Literature was used as basis for preliminary assessment in H₂













Engineering Calculations



Fatigue



Calculations

- Remaining life based on historical cycling
- Maximum cycling for a 100-year life

Defect Cases

- Infinitely long internal defect surviving hydrotest
- Semi-elliptical defect surviving hydrotest
- ASME B31.12 semi-elliptical defect
 - Assumed toughness:
 - 100 Mpa.m^{0.5} in air
 - 50 Mpa.m^{0.5} in H₂

Outputs

- For largest defect to survive hydrotest:
 - Cycling at 1.5 MPa daily is permissible for design life of 100 years at current MAOP
 - Based on historical cycling fatigue life is
 >1000 years in all cases

	Initial defect		Life with current	Maximum cycling for	
Case	Depth [mm]	Length [mm]	cycling	a 100 year life	
1	1.31	Inf. Length	Historical cycling	2.11 MPa daily cycle	
	(max hydrotest defect)		H ₂ : 3,400 years	H ₂ : 100 years	
			Air: 119,000 years	Air: 792 years	
2	2.36	50	Historical cycling	1.58 MPa daily cycle	
	(max hydrotest defect)		H ₂ : 1,392 years	H ₂ : 100 years	
			Air: 62,056 years	Air: 1,029 years	
3	1.44	8.4	Historical cycling	5.28 MPa daily cycle	
	(ASME B31.12 defect)		H ₂ : 45,840 years	H ₂ : 100 years	
			Air:1,023,000 years	Air: 2,180 years	





Fracture Initiation & Propagation



Initiation

Calculations

- Max. axial through-wall CDL for different pressures
- Calcs based on AS 2885.1 Cl 5.5.4 and API 579
 - assuming 50% loss of toughness in hydrogen

Outputs

• 20% CDL reduction in the BM for all wall thicknesses

Coco	CDL (mm) at internal pressure of			
Case	4.5 MPa(g)	5.6 MPa(g)	10.6 MPa(g)	
Wall thickness 5.56 mm				
High toughness	164	125	44	
30 J (pipe metal)	150	119	44	
15 J (pipe metal with H ₂)	128	104	N/A	
10 J (weld)	114	93	39	
5 J (weld - with H ₂)	91	74	N/A	

Propagation

Calculations

Minimum required CVN for RDF control

Cases

• NG, $10\% H_2$, $100\% H_2$, at 3 pressures

Outputs

Req fracture arrest energy decrease in H₂

Pressure [MPa(g)]	Minimum required CVN FSE energy [J]		
	Pure methane	10% H ₂	Pure H ₂
4.5	10.4	9.7	3.8
5.6	14.5	13.4	5.4





Conclusions & Outlook

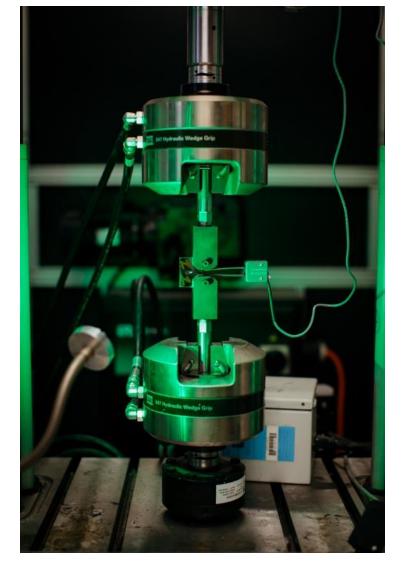


Conclusions & Outlook



Phase 1 works indicate the PGP will be suitable for 100% H₂ service

- No service pressure de-rating will be required
- Conversion capacity of 20-50TJ/day achievable
- Safely cycled to about 1.5 MPa/day
- The existing pipeline safety management is altered due to inclusion of hydrogen (e.g. failure mode change)
- Phase 1 results provided confidence for the project to progress to Phase 2 detailed testing and conversion planning







Overview





Introduction of hydrogen testing

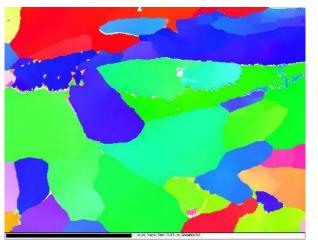
- 5.6 MPa(g)
- Other scenarios for some tests

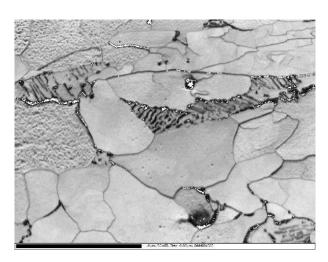
Material Characterisation

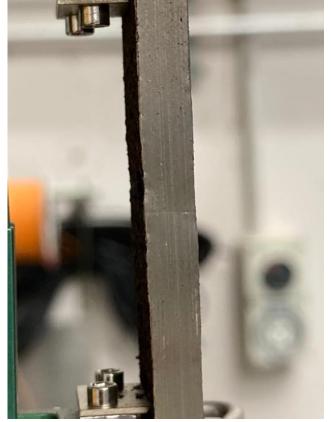
- More Detailed Analysis
- Inclusion & Grain Analysis

Strength

- Base Metal Circumferential & Longitudinal Tensile Tests [H₂]
- Cross Seam & Girth Weld Tensile Tests [H₂]















3-Point Bend Tests (Static Fracture)

Base Metal Circumferential & Longitudinal 3-Point Bend Test [air & H₂]

Combined Fracture Toughness & Fatigue

- Base Metal Circumferential & Longitudinal C(T) Tests [H₂]
- Cross Seam Weld C(T) Tests [air & H₂]
- Cross Girth Weld C(T) Tests in the HAZ & WCL [H₂]





Round Robin

- Sandia National Testing Labs
- Base Metal Circumferential & Longitudinal C(T) Tests [H₂]
- Cross Girth Weld C(T) Tests in the HAZ & WCL [H₂]

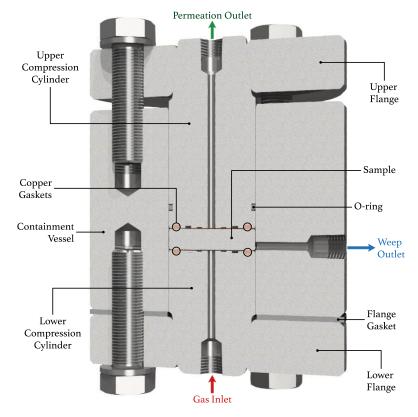
Permeation

- Multiple pressures and holding times
- Determine time to H₂ saturation
- Compare with fully submerged specimens

High-Strain Rate Testing

- Split Hopkinson Pressure Bar
- Pre-charged H₂ specimens











Laboratory Testing





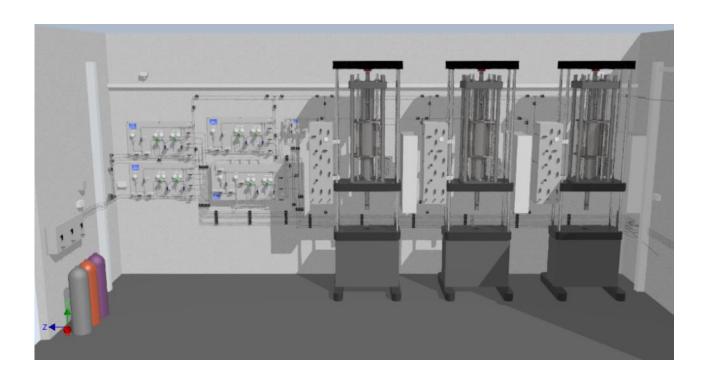


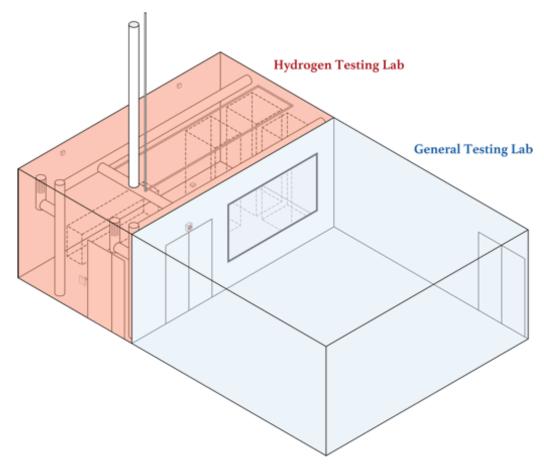












Test pressure up to 200 bar @ RT





Minimise Volume

- Max volume of hydrogen at any time in the lab
 <50% of the LEL (i.e. 2% v/v)
- Generally H₂ volume <25% v/v

Active Ventilation

- Continuous exchange with fresh air pumped in (> 4 air exchanges per hour)
- Can be manually switched to higher exchange rate

Continuous Monitoring

- ○O₂ and H₂ continuously measured
- Fed to centralised system

Centralised Purge Line

 All vessel contents can be purged to a central line that exhaust gases to atmosphere above roof

3rd Party Hazardous Assessment

Certified as a Non-Hazardous Area

































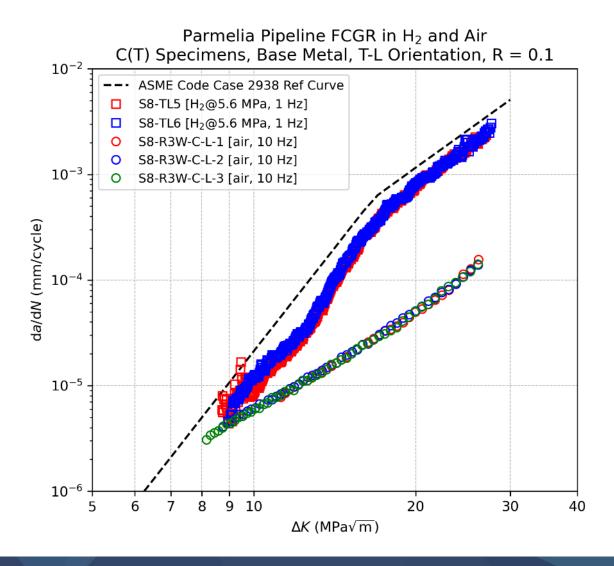
Round Robin Testing





Fatigue





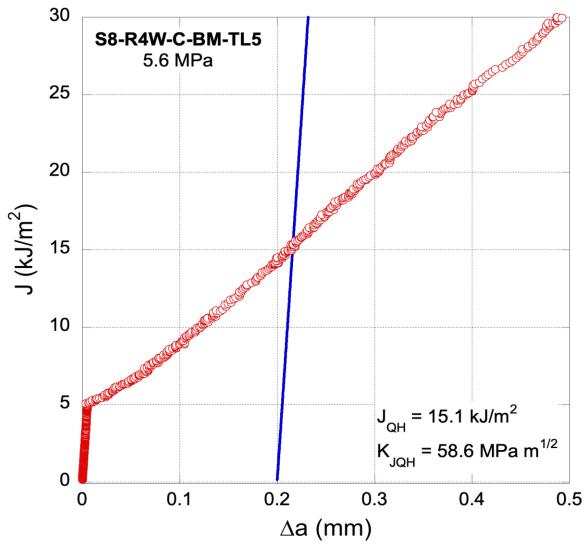
- So far two tests in H₂ @ 5.6 MPa
- Combined fatigue and fracture resistance
- Good repeatability
- Challenges observed during air (UOW) testing also showed up for H₂ testing (Sandia)

Fatigue

- Ref. curve from ASME Code Case 2938 provides a conservative prediction of the material performance at this R ratio and pressure
- Support the preliminary engineering calculations conducted in Phase 1 of the project based on expected material behaviour.

Fracture Resistance





Fracture Resistance

- 118 MPa.m $^{0.5}$ (air) to 58 MPa.m $^{0.5}$ (H₂)
- Loss of 50%
- Met ASME B31.12 requirement of 55 MPa.m^{0.5}





Conclusions & Outlook





Conclusions & Outlook



- Hydrogen testing in the H2SAFE(TI) Lab @ UOW begins in June
- Project runs until December 2022
- Update Engineering Assessment
- Refine Safety Management Study
- Prepare Conversion Design Basis
- Inform Regulatory and Stakeholder Engagement
- Results will be disseminated in future proceedings



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Thank you for your attention.